

IPRO 302

Zero Liquid Discharge



HYDROPURE

Clean Water. Clean Energy. Clean Living.

Sponsored by:

Sargent & Lundy^{LLC}

Overview

- Problem
- Project
- Goals
- Water Balance
- Options/Cases
- Final Costs
- Conclusion



Visit to Midwest Generation Plant

Our Problem

- Finding the most economical Zero Liquid Discharge system
 - It is difficult to obtain permits to discharge process waste water from facilities that generate electricity.
 - How can we eliminate the power plant's waste water discharge stream?

Team Organization

Advisors: Don Chmielewski, Myron Gottlieb Sponsor: Sargent & Lundy

Team Leader: William Pattermann

Preliminary Research Teams

- 1. Evaporation Pond**
 - Angela Ng (L)
 - Alex Ong
 - Danny Beissinger
- 2. Deep Well**
 - Will Pattermann (L)
 - James Lai
 - Mitchell Isoda
- 3. Brine Concentrator**
 - Ray Ballard (L)
 - Sahar Ashrafi
 - Woo Sung Shin
- 4. Emerging Technology**
 - Ross Hill (L)
 - Catherine Latour

Extensive Research Teams

- 1. Physical Team**
 - Alex Ong (L)
 - Angela Ng
 - Woosung Shin
- 2. Regulatory Team**
 - James Lai (L)
 - Danny Beissinger
- 3. Technological Team**
 - Sahar Ashrafi (L)
 - Ray Ballard
 - Catherine Latour
- 4. Financial Team**
 - Mitchell Isoda (L)
 - Ross Hill

Final Teams

- 1. Final Presentation Team**
 - Ray Ballard (L)
 - Angela Ng
 - Will Pattermann
 - Ross Hill
- 2. Final Report Team**
 - Sahar Ashrafi (L)
 - Mitchell Isoda
 - Catherine Latour
- 3. Poster Team**
 - Danny Beissinger (L)
 - Woosung Shin
- 4. Brochure Team**
 - Alex Ong (L)
 - James Lai

Project Challenges

- Fully understanding the problem given by Sargent & Lundy
- Difficulty finding extensive research
- Finding the time to do all research and presentations

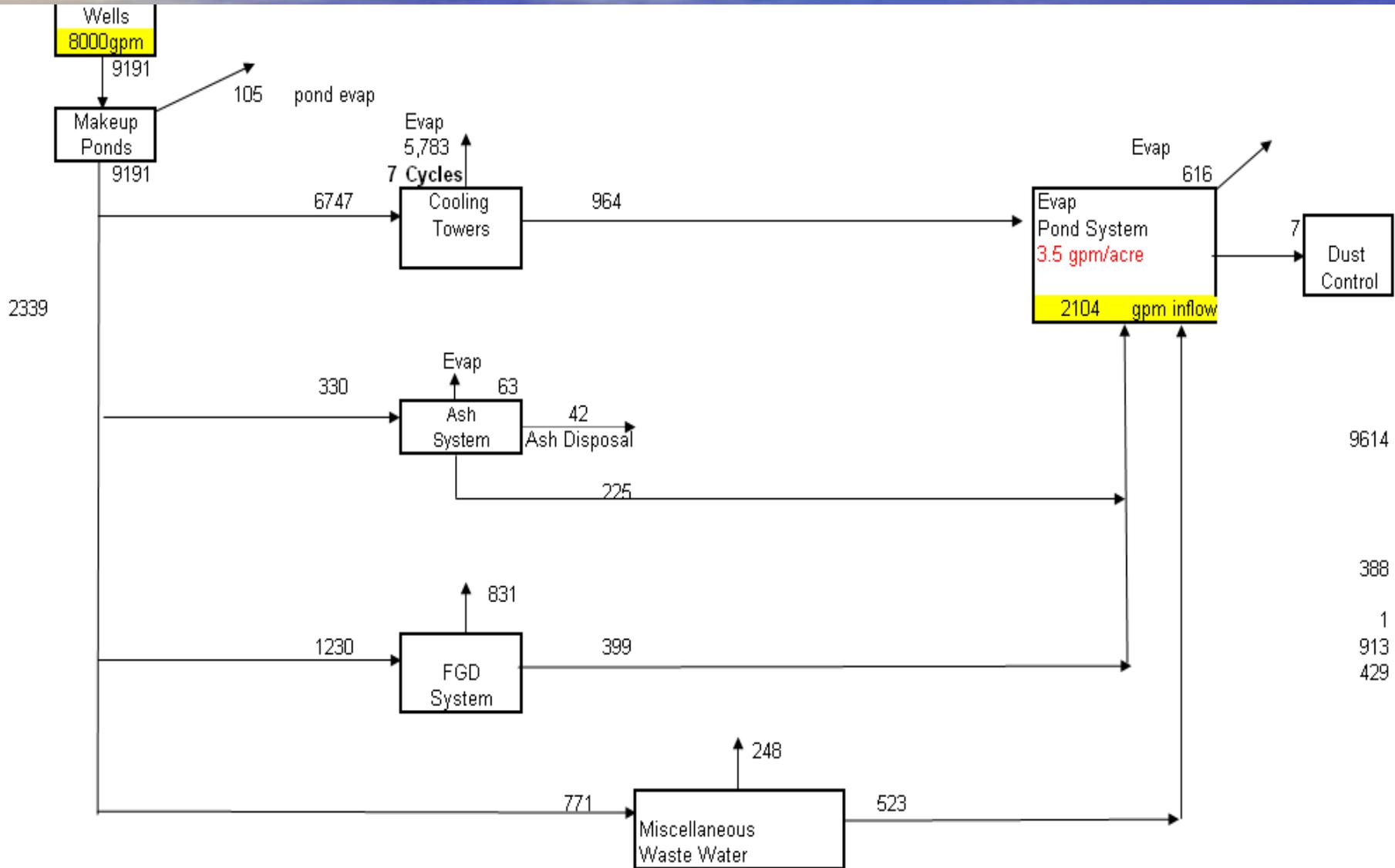
Team Ethical Challenges

- How to deal with uncooperative team members
- Determining how in depth research should be distributed
- Communication among members

Our Goal

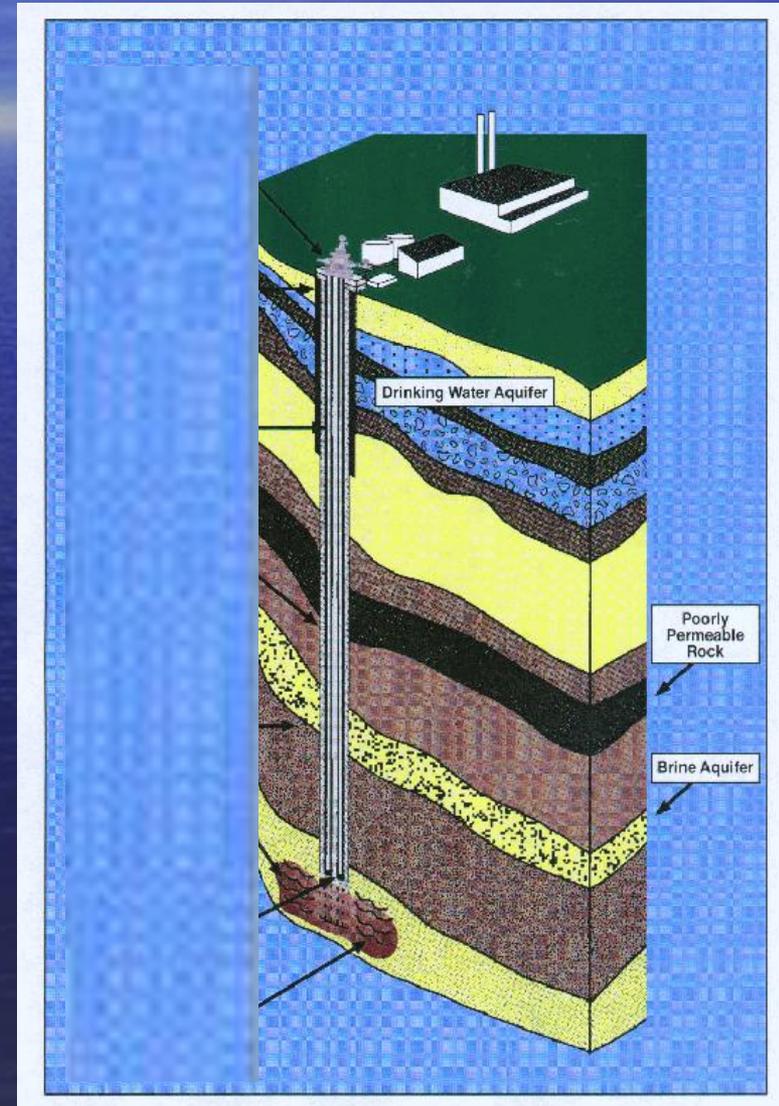
- Identify, evaluate, and prioritize technologies that can be used to eliminate waste water output
 - Water balance of power plant in Nevada
 - Finding options for reusing and treating discharge water
 - Size, capital cost and operating cost

Water Balance Assumptions



Deep Well

- **Definition:** Man-made wells to inject fluid into the ground, either for disposal or to extract other material from the ground.
- **Goal:** Assess how a deep well could help reduce waste water discharge from a coal power plant.
- **Resolution:** Deep wells are not a feasible solution for zero discharge in Nevada --- all possible injection wells are prohibited by Nevada law

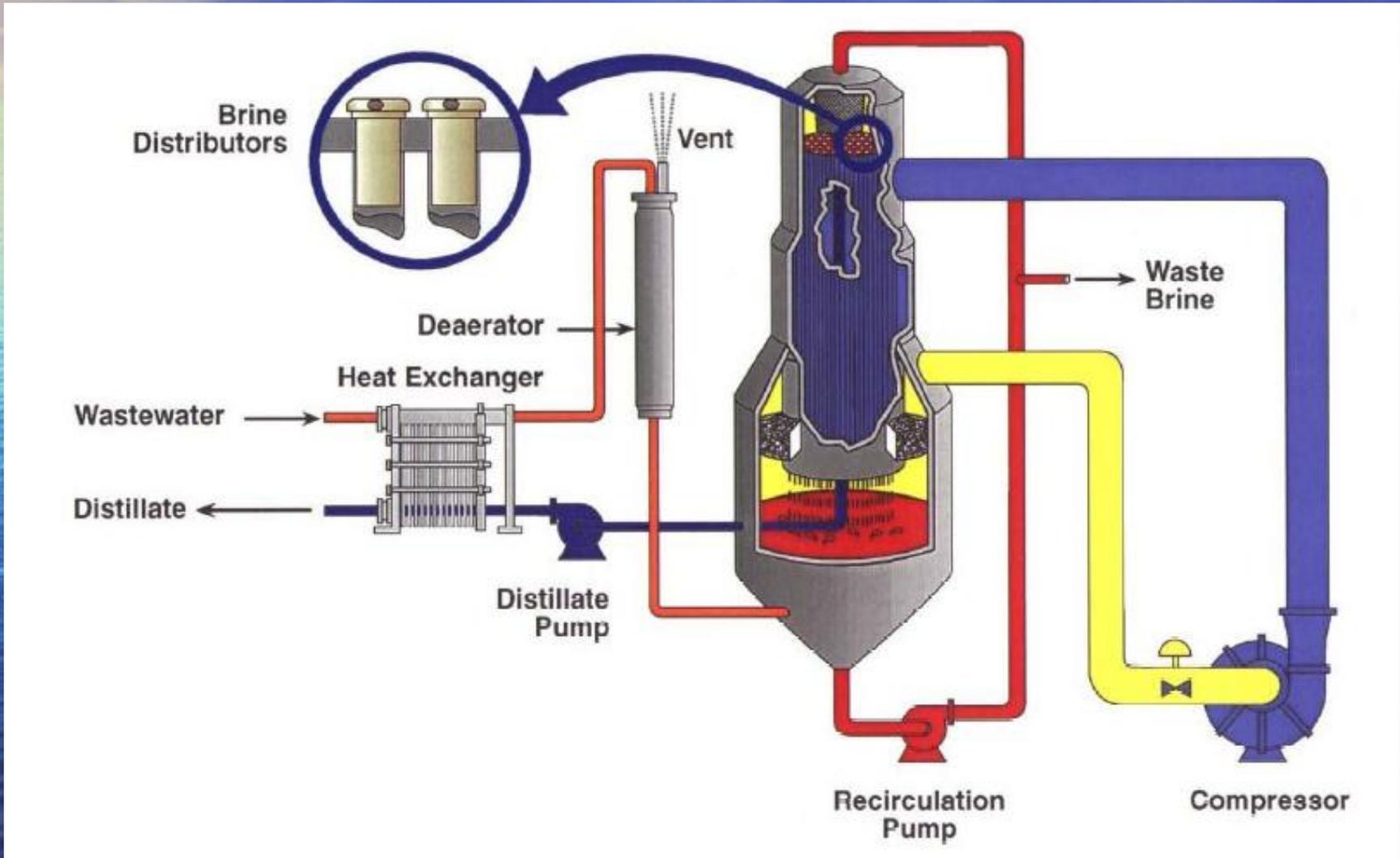


Evaporation Pond

- **Definition:** Shallow dugout with very large surface areas to evaporate water by sunlight and exposure to ambient temperatures.
- **Pros:**
 - Relatively cheap compared to other technologies
 - Easy to maintain
- **Cons:**
 - Land consuming
 - Threaten wildlife
 - Low feasibility
 - Lining cost



Brine Concentrator



Brine Concentrator

(Vapor Recompression Evaporator)

- **Definition:** Takes waste water and separates it into outlet streams of clean water and sludge
- **Pros:**
 - Recovers 95% of plant wastewater
- **Cons:**
 - High capital Costs
 - High maintenance costs



Reverse Osmosis (RO)

- Definition: Membrane based filtration system used to separate waste system into clean water and concentrated sludge
- Pros:
 - Minimal maintenance
 - 40%–60% of water recovery per unit
 - Low risk of malfunction
- Cons:
 - High initial cost
 - Membrane clogging



Evaporation Pond

- Design equation
 - Amount of water entering/evaporation rate = A
 - Depth of pond = 3 ft = D
 - Total Area = $1.2 * A (1 + 0.155 * D) / \sqrt{A}$
- Total Design Cost
 - land area
 - drainage pump and pipe
 - primary 80 mil, geonet, and secondary 60 mil liners
 - Bird netting; turtle & perimeter fencing



Brine Concentrator

- Compressor & Evaporator
 - Cost based on the flow needed

- Design Constants
 - Used to calculate other costs

$$C_b := e^{[7.2223 + 0.8(\ln(PC))]}$$

$$C_s := 10,800 * A^{[0.55]}$$

$$C_p := F_d * F_m * C_b$$

- Total Design Cost
 - Capital Cost
 - Materials
 - Labor
 - Indirect Expenses
 - Construction Prices
 - Contractor Expenses

Reverse Osmosis

- Based on flow needs
- Design equation
 - from Perry's Chemical Engineers' Handbook
 - $\$E = (0.724 - 1000) \times (\Delta P) (\$/\text{kWh}) / (CR)(Ef)$
 - $\$A = (0.423)(\$/\text{m}^2) / CR - J - T$
 - Total operating cost = $\$A + \E
- Total Design Cost
 - Capital
 - Operating
 - Installation
 - Material/piping

Case Options 1

Existing Evaporation Pond

Case 1

Recycle/Reuse

New Evaporation Pond



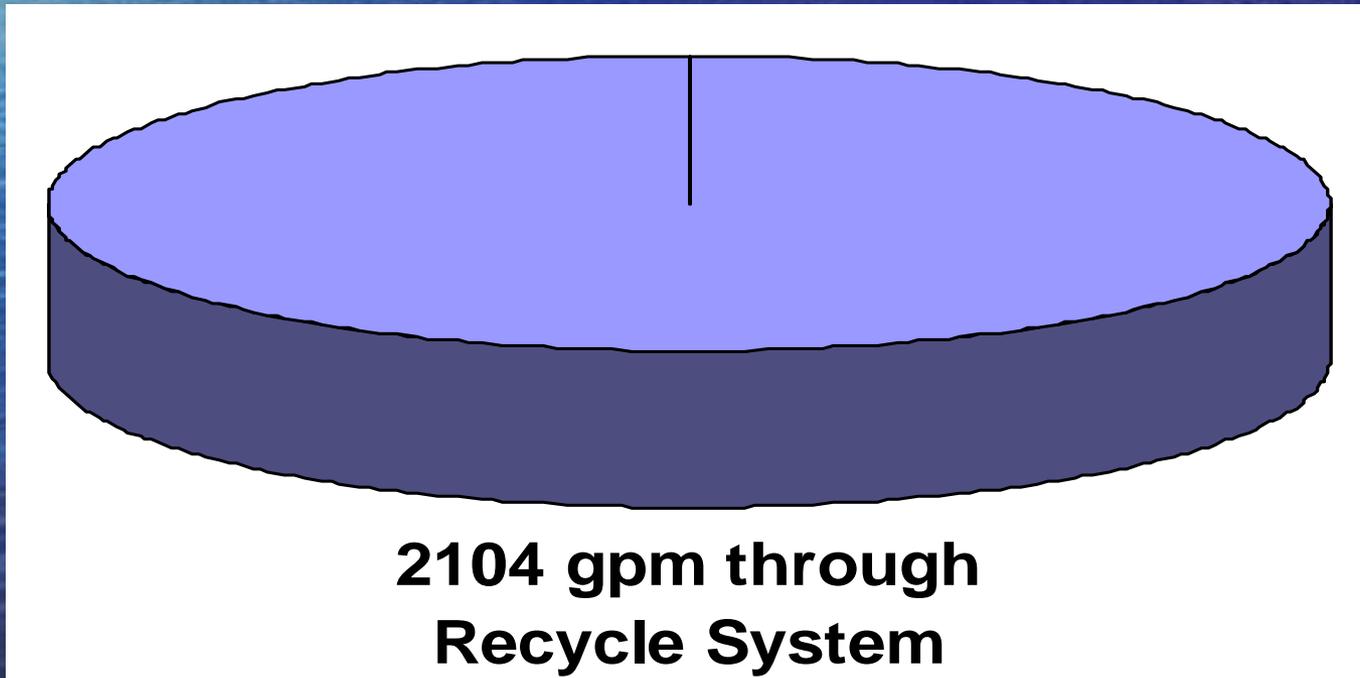
Case Scenario 1

Case 1

Reverse Osmosis =
\$122,280,924

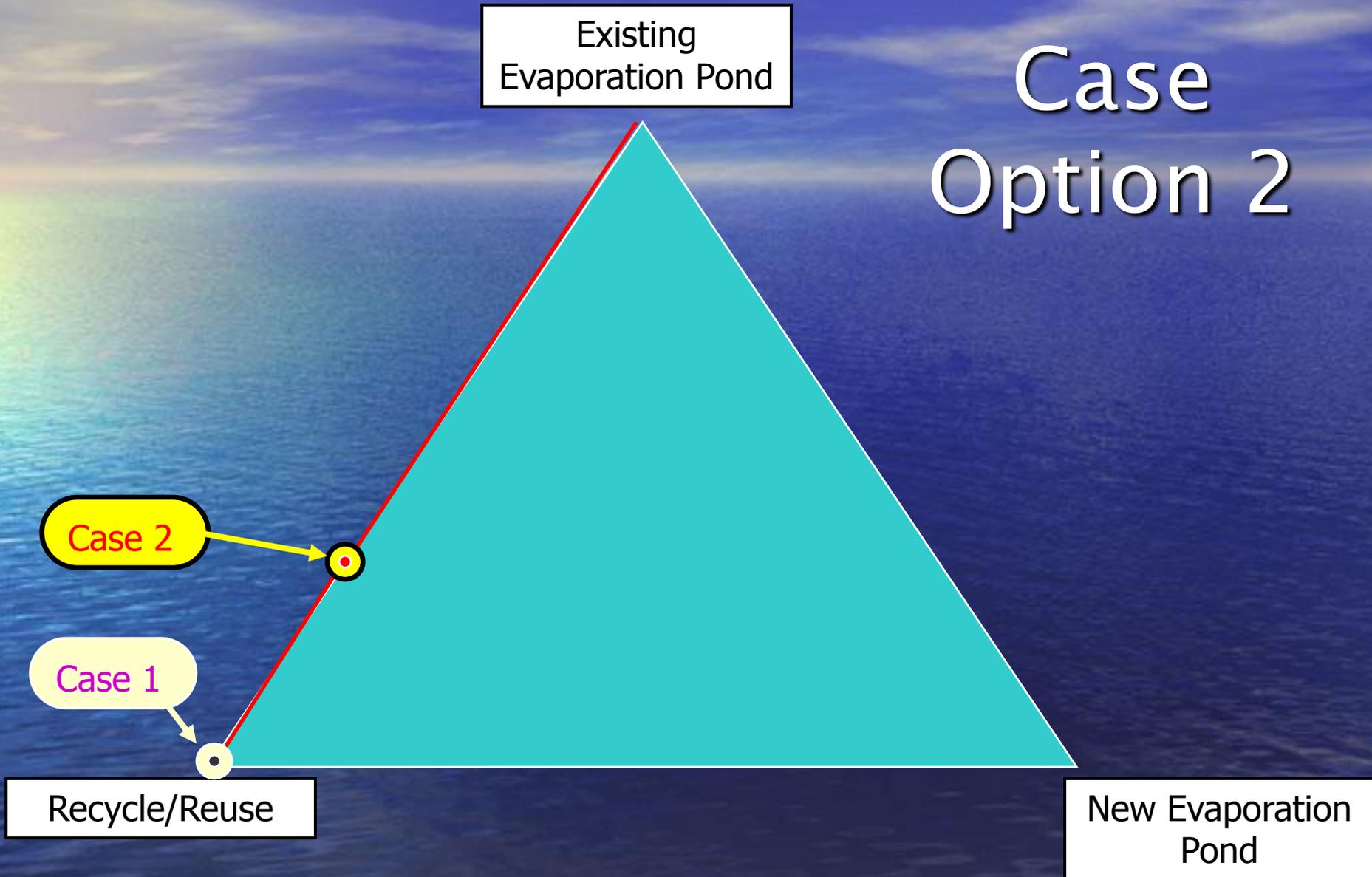
Brine concentrator =
\$175,442,083

Evaporation Pond = \$0



Interest
Rate:
12%
APR,
Life: 15
years

Case Option 2



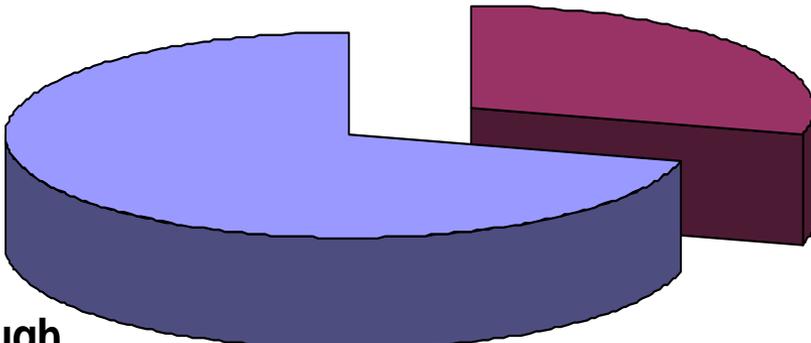
Case Scenario 2

Case 2

Reverse Osmosis =
\$86,480,045

Brine concentrator =
\$133,239,424

Evaporation Pond = \$0

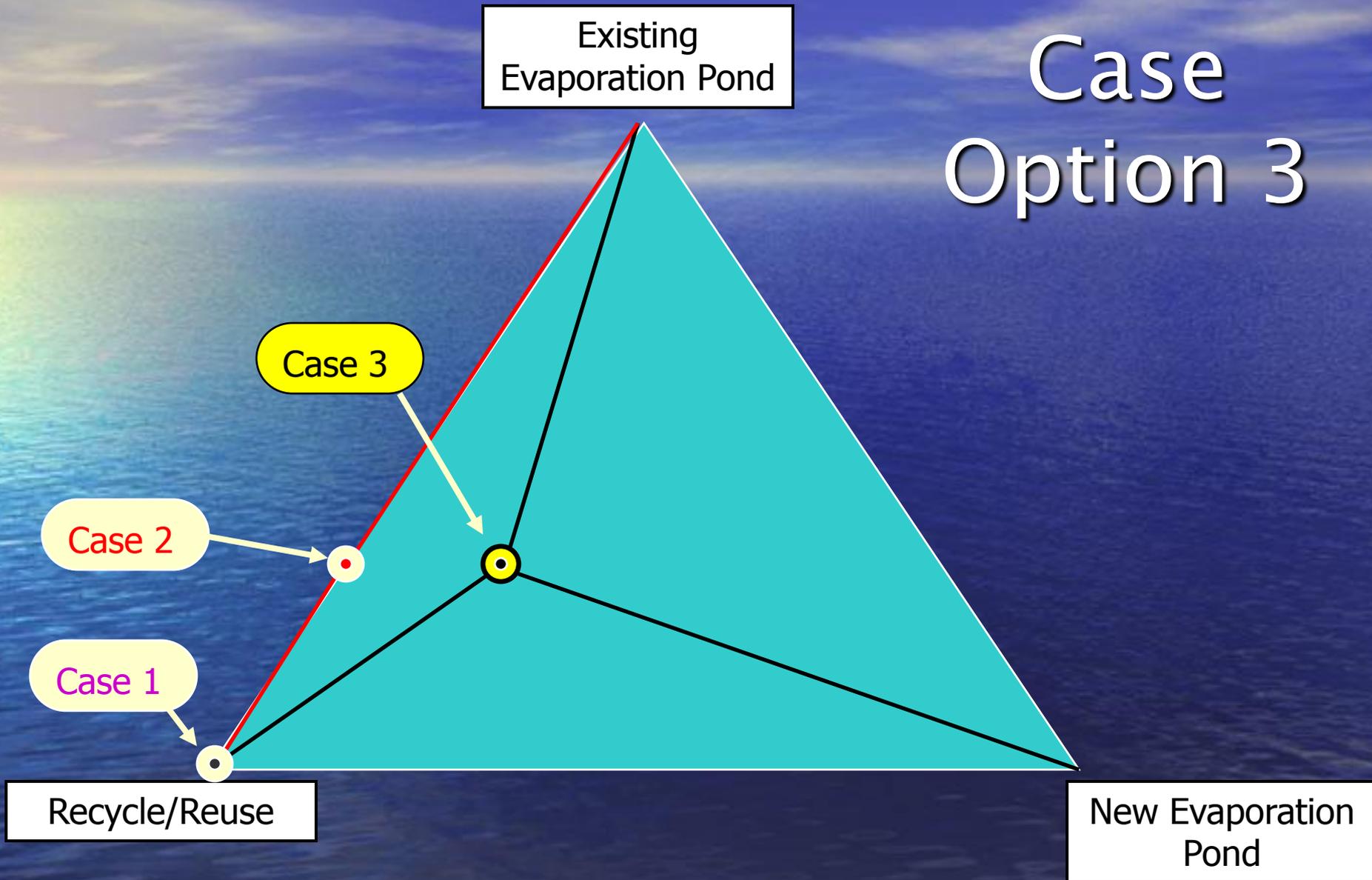


1488 gpm through
Recycle System

616 gpm to
existing Evap.
Pond

Interest
Rate:
12%
APR,
Life: 15
years

Case Option 3



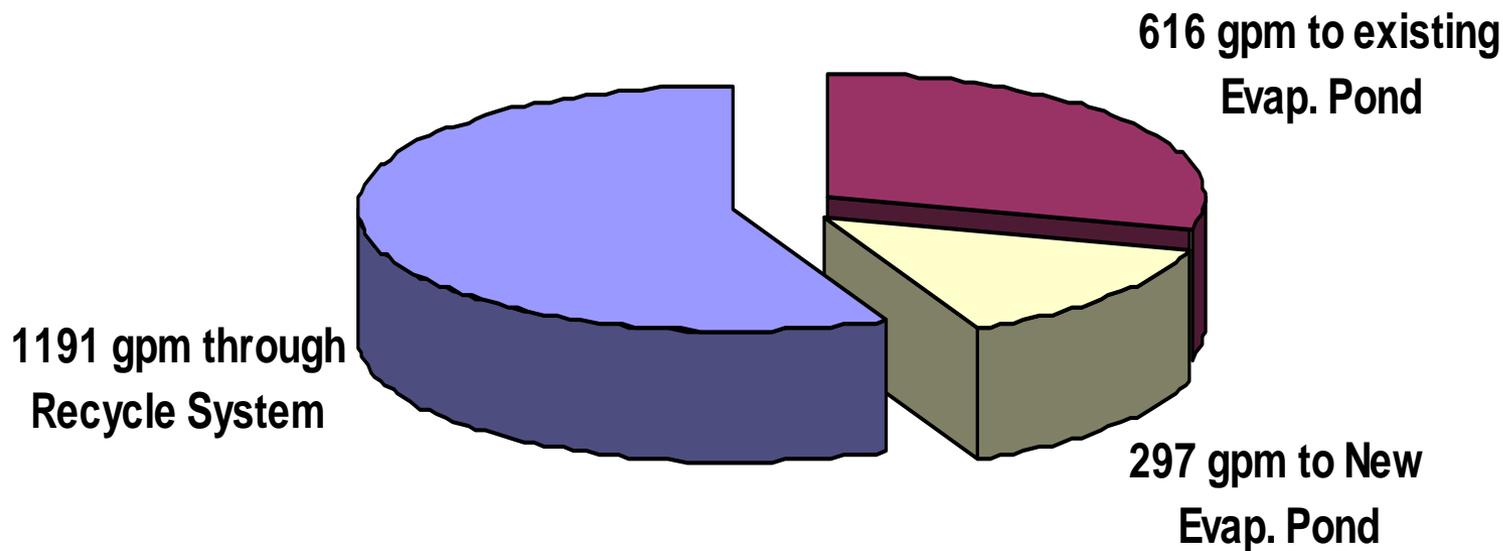
Case Scenario 3

Case 3

Reverse Osmosis =
\$69,218,907

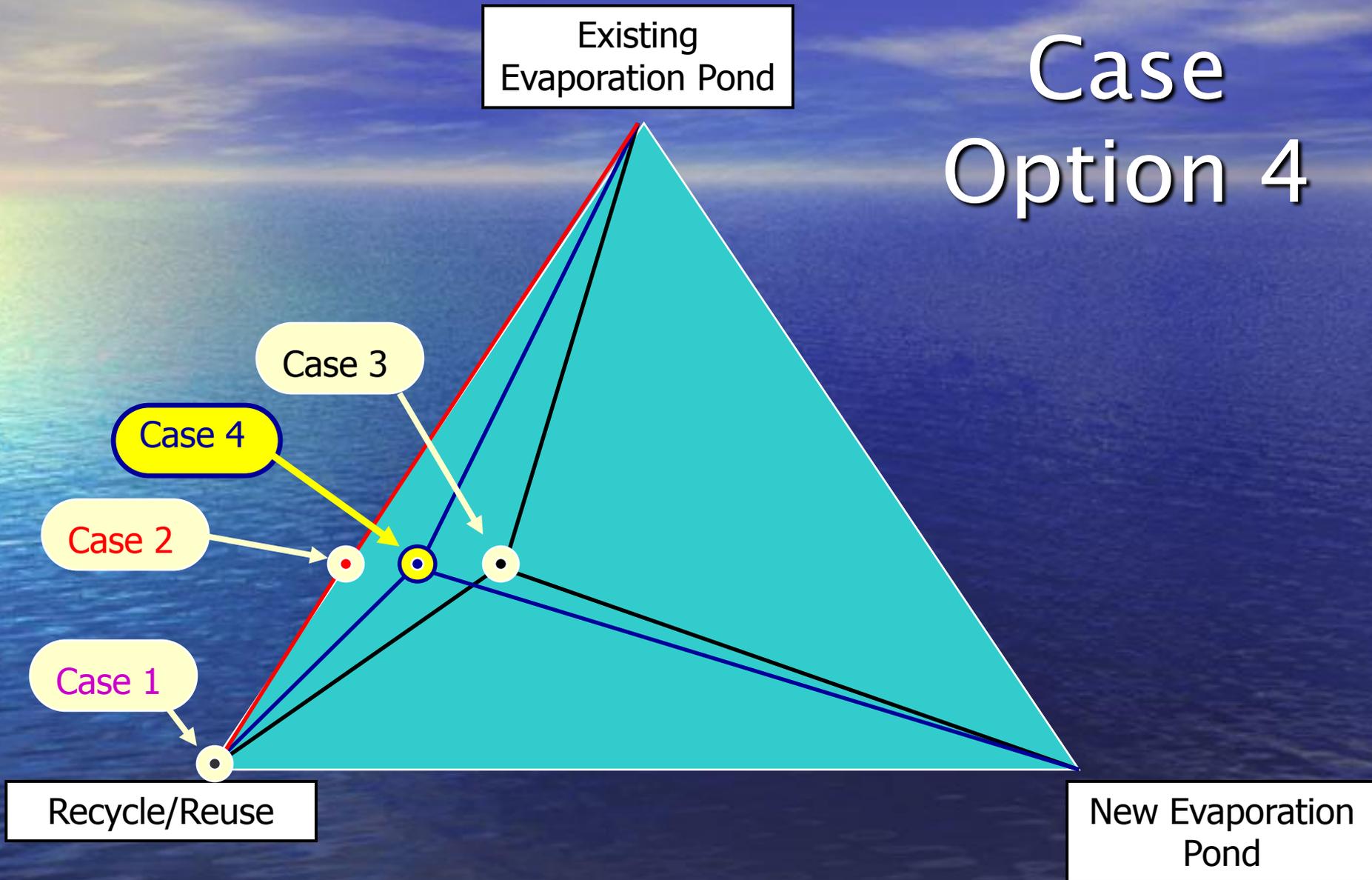
Brine concentrator =
\$111,652,263

Evaporation Pond = \$2,292,282



Interest
Rate:
12%
APR,
Life: 15
years

Case Option 4



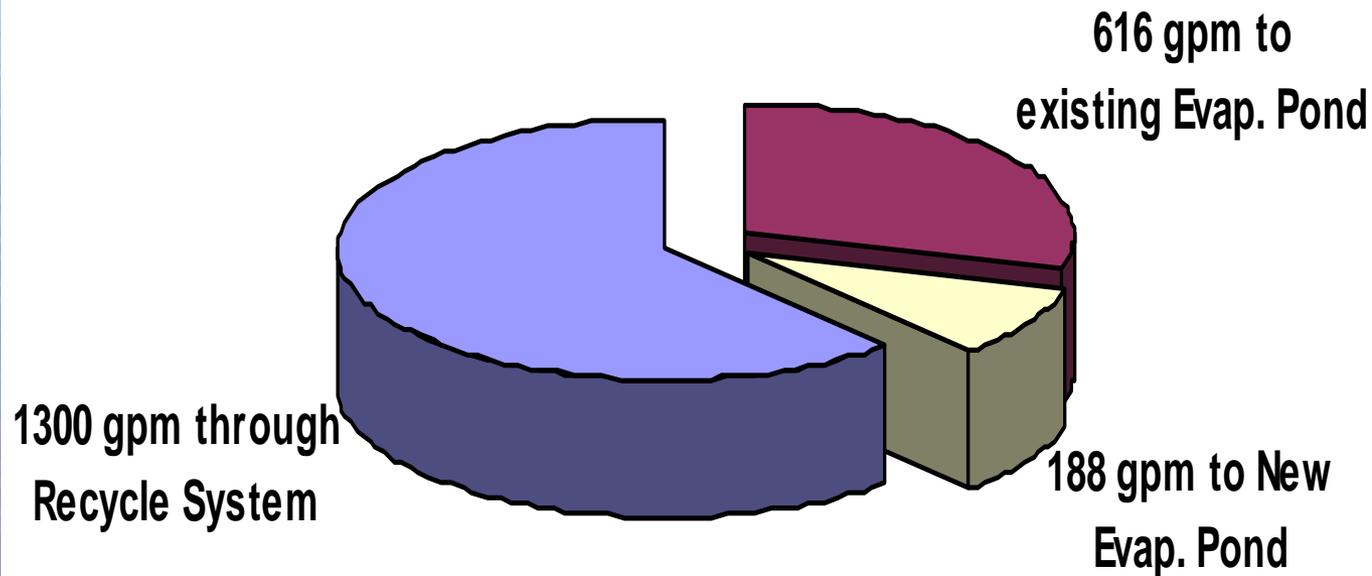
Case Scenario 4

Case 4

Reverse Osmosis =
\$75,533,803

Brine concentrator =
\$119,689,985

Evaporation Pond = \$1,841,824



Interest
Rate:
12%
APR,
Life: 15
years

Conclusion

- Best cost case scenario is Case 3
 - Use a Reverse Osmosis recycle system to recycle 1191 gpm of wastewater
 - Use the original evaporation pond of 616 gpm and create an additional evaporation pond for 297 gpm of wastewater

Total Cost: \$71,511,189

Our IPRO Family

- Expectations
- IPRO Experience
- What We Learned

Any Questions?